



Modelling and Computation of Dynamic Phase Transition of Liquids - Compressible Flows with Cavitation -







	Outline	
•	Introduction	Important numbers
		Physical effekts
	Modeling	CATUM Cavitation Technische Universität München
	Numerical results and validation	- Spherical body:
		- Hydrofoil
		- Prismatic body – cavitation erosion





Physics of cavitating flows

Dominating

- strong density variation $\rho_l / \rho_v \approx 10^4$
- strong variation of speed of sound $c_l/c_{min} \approx 10^3$
- coexistence of compressible and weak compressible flow regimes
- formation of violent shocks in collapse region
- intense noise, vibration and erosion



p





 $p_{s,\infty}$ coexistence of phases equilibrium

metastable time scale of flow

Cavitation dynamics

1. Process

Depressurization - evaporation increase of volume - 1 : 50000 displacement of liquid fluid instability

2. Process

collapse implosion of bubbles and cavitation patterns violent shocks erosion

Compressibility

local very low wave speed $c \le 10$ m/s stiffness because of coupling with regimes of $c \approx 1500$ m/s





Nucleation

Homogeneous

Heterogeneous

Nucleus consists of molecules

Exclusive hom. nucleation allows high surface tention and highly metastable states

Only important with pure water

Impurities like dissolved gas or crevices at walls or particles act as nucleus

Dominant in most technical applications





Cavitation phenomena



Bubble and cloud cavitation



Sheet and cloud cavitation



Supercavitation



Vortex cavitation





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Size of cavitation structures



Sphere diameter Size of a fluidemement d_{sphere}=1,5 10⁻¹ m d_{element}=5,2 10⁻³m







Two-phase flow properties via integral averages per cell



 $\alpha_{cell1} = \alpha_{cell2} = \alpha_{cell3}$

subgrid scale structures \rightarrow integral average properties (FVM)

$$\overline{\rho} = \frac{1}{V_{cell}} \int_{V_{cell}} \rho \cdot dV \qquad \qquad \overline{\rho u} = \frac{1}{V_{cell}} \int_{V_{cell}} \rho u \cdot dV \qquad \qquad \overline{\rho E} = \frac{1}{V_{cell}} \int_{V_{cell}} \rho E \cdot dV$$

Stable thermodynamic conditions \rightarrow constitutive relations (EOS) determine cell variables \overline{p} , \overline{T}

$$\implies \overline{\rho} = \overline{\rho}(\overline{p}, \overline{T}) \qquad \overline{e} = \overline{e}(\overline{p}, \overline{T})$$





Thermodynamic Equilibrium Conditions - Substitute EOS

- "Equation of state" for liquid water: modified Tait "EOS" (thermal and caloric EOS for pure liquids)

$$\overline{p}(\overline{\rho},\overline{T}) = (B + p_{sat}(\overline{T})) \cdot \left(\frac{\overline{\rho}}{\rho_{l,sat}(\overline{T})}\right)^n - B$$
$$e_l(\overline{T}) = c_{vl} \cdot (\overline{T} - T_{ref}) + e_{l,ref}$$

- EOS of pure water vapour: perfect gas law (thermal and caloric description of pure vapour)

$$\overline{p}(\overline{\rho},\overline{T}) = \overline{\rho} \cdot R_{v} \cdot \overline{T}$$
$$e_{v}(\overline{T}) = c_{vv} \cdot (\overline{T} - T_{ref}) + e_{v,ref} + l_{v}$$

For water: $B \approx 3.3 \cdot 10^8$ Pa, $n \approx 7.15$, reference state ref.: expected mean temperature (293.15 K).

-EOS for saturated water/vapour: saturation conditions – Oldenbourg polynomials (conditions for saturated mixture of water and water vapour for a void fraction α)

$$\overline{p} = p_{sat}(\overline{T})$$

$$\overline{\rho} = \alpha \cdot \rho_{v,sat}(\overline{T}) + (1 - \alpha) \cdot \rho_{l,sat}(\overline{T})$$

$$\overline{\rho e} = \alpha \cdot \rho_{v,sat}(\overline{T}) \cdot e_v(\overline{T}) + (1 - \alpha) \cdot \rho_{l,sat}(\overline{T}) \cdot e_l(\overline{T}).$$





Thermodynamic model - EOS saturation curve 10⁸ combined EOS at T = 293 K IAPWS data at T = 293 K 10⁷ Combined EOS contains relations for: 10⁶ \rightarrow modified Tait equation - pure water [b] 10⁵ d - vapour phase \rightarrow ideal gas law - two-phase region \rightarrow saturation conditions 10⁴ $p_{sat}(T_{sat})$ T_{sat} 10³ 10² 10⁻² 10⁻³ 10⁻¹ 10⁰ 10² 10³ 10¹ $v [m^3/kg]$





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Finite volume Method

Compressible, frictionless, unsteady flows -> Euler equations

Grid: structured hexagonal cells

Flux function: density based

Solver: mod. Riemann solver

2nd order accurate

explicit





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Numerical results – application: two-phase flow

3-D simulation of Branders experiment of cavitation around a sphere







Numerical results – application: two-phase flow

Comparison of two-phase structures experiment/simulation



Experiment: Brandner, P. A., Walker, G. J., Niekamp, P. N. and Anderson, B., "An Investigation of Cloud Cavitation about a Sphere." In: 16th Australasian Fluid Mechanics Conference, 2 – 7 December 2007, Crown Placa, Gold Coast, Australia, 2007.



Simulation CATUM: Isosurfaces α =0.05, one instant in time.











2.4·10⁷ cells 6·10⁵ time steps, $\Delta t \approx 5 \cdot 10^{-8}$ s,





Numerical results – 2-D hydrofoil



 Δt_{movie} = 3·10⁻² s

 $2.4 \cdot 10^7$ cells, $6 \cdot 10^5$ time steps, $\Delta t \approx 5 \cdot 10^{-8}$ s, 96/192 CPU (Ix64a Opteron) → 500 h





Numerical results – fragmentation of two-phase flow

2-D cavitation on 2-D hydrofoil



Effect of the spatial resolution on the structures of the vapor volume fraction $\boldsymbol{\alpha}$





Numerical results – fragmentation of two-phase flow

2-D cavitation on 2-D hydrofoil



Effect of the spatial resolution on the instantaneous maximum loads – pressure footprint over one cycle





Numerical results – fragmentation of two-phase flow



2-D cavitation on 2-D hydrofoil

Effect of the spatial resolution on the instantaneous maximum loads – pressure footprint over one cycle, **zooms of previous pictures**





2-D hydrofoil – maximum pressure



Collaps induced maximum pressure on the suction side - $p_{max} \approx 2000$ bar Analysed time: one period with $\Delta t_{zyklus} = 10^{-2}$ s



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Cavitation erosion



Kuiper, G. - MARIN Maritime Research Institute - The Netherlands









Driving mechanisms of cavitation erosion







Single bubble collapse with wall interaction



J.P. Franc, J.M. Michel: "Fundamentals of Cavitation", 2004

Simulation CATUM

Initial radius R₀=0.5 mm, time step Δt_{CFD} =6.0·10⁻⁹ s, collapse time 1.7 ·10⁻⁵ s, Initial pressures p_{liquid}=10.0 bar, p_{bubble}=0.023 bar , T=293 K, water/vapor





3-D simulation of the "Obernach-experiment" on cavitation erosion







Dynamic phase-transition and related pressure field



Top view: Two-phase regions, Δt_{Movie} =0.17 s.

Perspective view: Two-phase regions and static pressure at the walls, Δt_{Movie} =0.17 s.





Comparison of two-phase structures experiment/simulation



Experiment: Huber R., Geschwindigkeitsmaßstabseffekte bei der Kavitationserosion in der Scherschicht nach prismatischen Kavitatoren, Berichte des Lehrstuhls und der Versuchsanstalt für Wasserbau und Wasserwirtschaft, Hrsg. Univ.-Prof. Dr.-Ing. Th. Strobl, Nr. 102, 2004.

Simulation CATUM: Isosurfaces α =0.01, one instant in time.





Fragmentation of two-phase structure, collapse, shock formation





 $\Delta t_{1 \rightarrow 2}$ =1.17·10⁻⁴ s $\Delta t_{2 \rightarrow 3}$ =0.58·10⁻⁴ s







Areas of intense erosion (experiment) - maximum pressures (simulation)



Experiment: Huber R., Geschwindigkeitsmaßstabseffekte bei der Kavitationserosion in der Scherschicht nach prismatischen Kavitatoren, Berichte des Lehrstuhls und der Versuchsanstalt für Wasserbau und Wasserwirtschaft, Hrsg. Univ.-Prof. Dr.-Ing. Th. Strobl, Nr. 102, 2004.

Simulation CATUM: Collapse induced maximum pressure at the bottom wall of the numerical test-section, analysis interval 0.058 seconds. Stars indicate the barycenters (experimental) of the erosion ares.





Discussion